

AMENDMENTS TO THE CLAIMS

1. (Currently Amended) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons and being essentially free of sulphur compounds, comprising hydrogenating in two steps a mainly olefinic liquid feed-stock comprising olefins, and sulphur compounds as impurities, in the presence of hydrogen and a noble metal catalyst on aluminium oxide support, wherein in the first step the major part of olefins are converted and in the secondary step the remaining olefins and sulphur compounds react, wherein a trickle-bed reactor is used in the first step and in the second step, wherein the feed-stock comprises 80-97 wt % of C₈ olefins, 3-20 wt % of C₁₂ olefins, and 0.1-7 wt % of C₉, C₁₀, C₁₁ and olefins heavier than C₁₂, [[and]] wherein the reaction temperature in the first step is in the range of 150-230°C and the pressure is in the range of 20-70 bar and in the second step the temperature is in the range of [[180-300°C]] 190-260°C and the pressure is in the range of 20-70 bar, wherein the reaction temperature in the second step is higher than the reaction temperature in the first step. [[and]] wherein the hydrogen feed/olefin feed molar ratio is from 0.9 to 2.0, and wherein the concentration of the noble metal in the noble metal catalyst is less than 1wt%.

2. (Cancelled)

3. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the feed-stock further comprises minor amounts of lighter C₆-C₇ olefins and 1-1000 wt-ppm of sulphur compounds, calculated as sulphur.

4. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the feed-stock originates from a mixture obtained from a dimerization of butenes.

5. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the feed-stock contains as sulphur compounds mainly sulphides, disulphides, thiophene and/or alkylthiophenes.

6. (Currently Amended) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the noble metal catalysts comprises [< 1 wt% of] platinum, palladium or a combination thereof ~~or and~~ palladium.

7. (Currently Amended) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the noble metal catalysts comprises [< 1 wt% of] platinum.

8. (Cancelled)

9. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1 wherein the reaction heat is removed from the process and the reaction heat is used for preheating of incoming feed-stock to the a dimerization unit of butenes, or as an energy source for distillation columns of bottom boilers of dimerization unit of butenes.

10. (Cancelled)

11. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein in the first step the product stream is circulated in the reactor(s).

12. (Previously Presented) A process for the manufacture of a gasoline blending component containing paraffinic hydrocarbons according to Claim 1, wherein the hydrogen feed /olefin feed molar ratio is 1.0-1.5.